#### Numerical Simulation of Cavitating Flows

Steffen Jebauer July 12<sup>th</sup> 2006

# Motivation

- Cavitation is complex process
- Not completely understood
- Hardly to predict
- Testing of existing models and combination with others → Validation
- Estimation of numerical errors

# Contents

- Cavitation modelling
  - Two-phase flow approach
  - Mass transfer model
  - Cavitation and cavitation inception
- Test cases
  - Two-dimensional
  - Three-dimensional
- Conclusion and outlook

# Cavitation

Definition

Rupture of a liquid due to pressure decrease at roughly constant temperature.

- Saturation pressure p<sub>s</sub>
- Problem

Rupture starts at inhomogenities in a liquid, so-called nuclei

- Lack of nuclei might postpone inception
- Integral measure by means of tensile strength  $\Delta p_t = \frac{2S}{\Delta n n}$

$$\Delta p_t = p_S - \frac{2S}{R_B}$$

# **Cavitation modelling**

- Large density differences between liquid and vapour
- Volume-of-Fluid method  $\rightarrow r_v$ ,  $r_l$
- Two-phase flow with source term  $\Gamma_{lv}$

$$\frac{\partial}{\partial t}(r_V\rho) + \frac{\partial}{\partial x_i}(r_V\rho u_i) = \Gamma_{lv}$$

Homogenic description → number of equations

$$\vec{u}_v = \vec{u}_l$$

# **Cavitation modelling**

Rayleigh-Plesset mass transfer model

$$\Gamma_{lv} = F_{evap} \frac{3r_{nuc}(1 - r_v)\rho_v}{R_B} \sqrt{\frac{2}{3} \frac{|p_s - p_B|}{\rho_l}} \cdot sgn(p_s - p_B)$$
  
$$\Gamma_{lv} = F_{cond} \frac{3r_v \rho_v}{R_B} \sqrt{\frac{2}{3} \frac{|p_s - p_B|}{\rho_l}} \cdot sgn(p_s - p_B)$$

- $F_{evap} = 50, F_{cond} = 0.01$
- $r_{nuc} = 5 \times 10^{-4}$ ,  $R_B = 2 \times 10^{-6}$  m

# **Turbulence modelling**

- RANS, URANS
- SST model, eddy viscosity model

$$\mu_t = \rho \frac{Ck}{f(\omega)}$$

• Blending via  $F_1$  function in  $\omega$ -equation between

$$-F_1 = 0 \rightarrow k - \varepsilon$$
 model, free stream

- $-F_1 = 1 \rightarrow k \omega \mod l$ , near walls
- Curvature correction to the SST model

$$P_k = f_r \cdot \widetilde{P}_k; \quad f_r = 0 \dots 1.25$$

# **Numerical errors**

- Errors regarding
  - Spatial discretisation
  - Time discretisation
  - Iteration number
- Time step studies
- Grid studies
- Abort at different residual norms

# Symbol definitions

Gas holdup

$$G = \int_{(v)} r_G \cdot dV$$

- Lift coefficient
- Pressure coefficient

$$c_L = \frac{2 \cdot F_L}{\rho_f \cdot u_\infty^2 \cdot A_P}$$

$$c_p = \frac{2 \cdot p_{stat}}{\rho_f \cdot u_\infty^2}$$

$$\sigma = \frac{2 \cdot (p - p_s)}{\rho_f \cdot u_\infty^2}$$

- $P_s$  Saturation pressure  $A_P$
- *P*<sub>stat</sub> Static pressure
- $u_{\infty}$  Inlet velocity
- $\rho_f$  Density water

- Hydrofoil surface
- $F_L$  Lift force
- $r_{v}$  Vapour volume fraction
  - $r_l$  Water volume fraction

#### **Two-dimensional test case**





# Boundary conditions Wall, free slip



Pressure boundary condition

$$p_{out} = \sigma \cdot \frac{\rho}{2} u_{\infty}^2 - p_s$$

# **Test Case Summary**

- Spatial discretisation

   HighResolution scheme, hybrid scheme
- Time discretisation
  - 2<sup>nd</sup> order Backward Euler
- Saturation pressure p<sub>s</sub>=3240 [Pa]
- Standard SST turbulence model
- Outlet: Pressure boundary condition via  $\sigma$
- Inlet: u<sub>∞</sub>=10 m/s, Re≈2×10<sup>6</sup>

Grids				
Grid	(1)	(2)	(3)	(4)
Node number	14 306	56 452	224 264	893 986
Element number	6 960	27 840	111 360	445 440
Min. grid angle [°]	40	41	38	43
First layer width y [µm]	20	10	5	2,5
Average layer width $y^+$	8	4	2	1
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# **Experimental data**

• Flow patterns in experiment





# Case study, $\alpha=0^{\circ}$

Pressure coefficient/ Vapour volume fraction



# Experimental data (2)

• Experiments Le et al. (1993)

– Pressure distributions



# Validation

#### • Pressure distribution on upper side:



#### **Pressure distribution**

• Angle of attack:  $\alpha$ =2.5° and 3.5°



URANS-Simulations, time averaged

#### **Threedimensional test case**

• Water test channel at SAFL (St. Anthony Falls Laboratory, Minnesota, U.S.A.)



### Geometry

• NACA 66<sub>2</sub>-415 profile





α...Angle of attack
 c<sub>0</sub>...Chord length
 b...half span

# Test case setup

- Spatial discretisation
  - HighResolution scheme for momentum
  - 1<sup>st</sup> order/ HighResolution for turbulence
- Time discretisation
  - 2<sup>nd</sup> order Backward Euler
- Single phase calculations, inception
- SST-model/ SST with curvature correction
- Inlet:  $u_{\infty} = 5.73...12.13$  m/s, Re=5.2×10<sup>5</sup>...1.1×10<sup>6</sup>
- Outlet: Pressure boundary condition via  $\boldsymbol{\sigma}$

#### Gitternetze Skalierfaktor 4<sup>1/3</sup> in jeder Raumrichtung × Grid Grob (1) Mittel (2) Fein (3) 358 519 5 442 459 Knotenanzahl 1 394 862 Elementanzahl 341 596 1 352 603 5 337 217 Wandschichtdicke y [µm] 30 15 7,5 Durchschnittl. Dicke $y^+$ 7,1 14,3 3,6

# Kavitationseinsatz

• Experimentelle Daten



# Lift

• Lift coefficient – Eff. angle of attack ( $\alpha$ - $\alpha_0$ )

• Experiment:  $Re_c = 9.2 \times 10^5$ 





#### Cut planes



### **Tip vortex**

- Medium(2) grid,  $\alpha_{eff}=12^{\circ}$ , Re=5.2×10<sup>5</sup>
- Different cut planes, vortex deflection



# **Tip vortex**

- Fine(3) grid,  $\alpha_{eff}$ =12°, Re=5.2×10<sup>5</sup>
- Model comparison



#### **Tip vortex**

- All grids,  $\alpha_{eff}$ =12°, Re=5.2×10<sup>5</sup>
- Small distance to blade tip



# **Cavitation inception**

• Decrease of  $\sigma$  according to:



# **Cavitation Inception**

Results and experimental values



# Summary

- Two-dimensional test case
  - Phase transition modelled
  - Averaged pressure distributions in good accordance
  - Transient behaviour detected
- Outlook
  - More experimental data
    - Vapour clouds
    - Volume fraction
  - Separation regions on foil surface

# Summary

- Threedimensional test case
  - Lift forces evaluated and compared (less grid influence)
  - Trailing vortex examined
  - Cavitation inception with single phase flow
- Outlook
  - Further grid refinement
  - Reynolds stress turbulence model
  - Pressure fluctuations

# Thank you very much for your attention.