



# Proceeding Paper Application of the Chemical Leaching Method for the Recovery of Li and Co Contained in Spent Li-Ion Batteries <sup>†</sup>

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Abstract: Waste batteries and accumulators are a group of waste, the amount of which is constantly increasing every year. A particular weight gain of this type of waste is observed for lithium-ion batteries used in various electronic devices and modern passenger vehicles. Due to the complex chemical composition and the content of different valuable metals, used Li-ion batteries should be subjected to appropriate recycling methods, the purpose of which is to separate the individual raw materials included in the battery. Regarding the demand for innovative technologies for processing spent Li-ion batteries, a concept of laboratory experiments was developed in the field of hydrometal-lurgical recovery of Li and Co contained in the battery powder obtained from this type of waste. As a result, it was shown that it is possible to effectively recover the tested metals with an adequately designed leaching process.

Keywords: Li-ion batteries; leaching; recovery of metals; waste management; environmental engineering

# 1. Introduction

Waste batteries and accumulators are a source of many raw materials, including metals necessary for producing various electrical and electronic equipment. Currently, the most popular type of batteries used in small-size portable electronic devices, as well as hybrid and electric vehicles, are lithium-ion batteries (Li-ion; LiBs), in which lithium and cobalt are included. These elements are also considered critical raw materials because they are indispensable components of the most modern technologies used worldwide and thus are overexploited forms of natural resources. As a result, such actions may lead to their rapid depletion, and the production of new products containing lithium and cobalt will be at risk. The solution to this problem is the use of secondary metallic materials contained in polymetallic waste, an example of which are spent Li-ion batteries. In industrial and laboratory practice, various techniques are used to recover metals in waste LiBs, including hydrometallurgical methods involving the leaching of elements from the battery powder into solution [1–5]. Thanks to the use of appropriate process parameters (i.e., the concentration and type of leaching and reducing agents, the ratio of solid to liquid phase, temperature, and the duration of experiments), it is possible to achieve high (over 95%) rates of metal recovery, including for Li and Co [5–12].

Considering the increased demand for the recovery of critical metallic raw materials (Li and Co) included in the waste Li-ion batteries, the concept of laboratory experiments in this field was developed.



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## 2. Materials and Methods

The research material was anode–cathode battery powder obtained due to the manual dismantling and fragmentation of spent Li-ion batteries contained in laptops of various brands. The tested powder was subjected to mineralization digestion in the presence of 65% HNO<sub>3</sub>, and the initial content of individual metals in the received solution was determined by the ICP-OES method.

For the separation of metals (namely, lithium and cobalt), the acidic reductive leaching method was applied. The conducted leaching experiments were performed in the presence of inorganic and/or organic leaching agents (i.e., sulfuric acid ( $H_2SO_4$ ), lactic acid ( $C_3H_6O_3$ ), and formic acid ( $CH_2O_2$ )). In addition, hydrogen peroxide ( $H_2O_2$ ) and glutaric acid ( $C_5H_8O_4$ ) were used as reducing agents. A list of other process parameters is presented in Table 1.

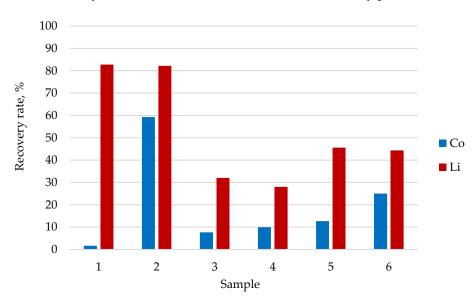
| Sample | Leaching Agent      | <b>Reducing Agent</b>                                    | Temperature | Solid/Liquid Ratio | Time    |
|--------|---------------------|--|-------------|--------------------|---------|
| 1      | 1.5 M sulfuric acid | 3 mL H <sub>2</sub> O <sub>2</sub>                       |             |                    |         |
| 2      | 1.5 M sulfuric acid | $3 \text{ mL H}_2\text{O}_2 + 5 \text{ g glutaric acid}$ |             |                    |         |
| 3      | 5 M lactic acid     | 3 mL H <sub>2</sub> O <sub>2</sub>                       | 90 °C       | 1/10               | 120 min |
| 4      | 5 M lactic acid     | 3 mL H <sub>2</sub> O <sub>2</sub> + 5 g glutaric acid   |             |                    |         |
| 5      | 5 M formic acid     | 3 mL H <sub>2</sub> O <sub>2</sub>                       |             |                    |         |
| 6      | 5 M formic acid     | $3 \text{ mL H}_2\text{O}_2 + 5 \text{ g glutaric acid}$ |             |                    |         |

**Table 1.** Determined parameters of the leaching process.

After leaching, the samples were vacuum filtered, obtaining solutions in which the content of tested metals was determined (ICP-OES method) and powdery leach residues, the latter of which were dried for 24 h at  $105 \,^{\circ}$ C.

#### 3. Results and Discussion

As a result of the leaching of the electrode powder from spent Li-ion batteries, acidic polymetallic solutions with a color from light pink to raspberry were obtained. The achieved results of the ICP-OES analyses are presented in Figure 1 in the form of percentage rates of metal recovery in relation to their initial content in the battery powder.



**Figure 1.** Recovery rates of Li and Co obtained as a result of acid leaching of electrode powder from spent Li-ion batteries.

The results of the Co and Li recovery rates indicate that the highest leaching of these two metals was simultaneously obtained in sample 2, where the sulfuric acid was used as leaching agent and the reducing agents were  $H_2O_2$ , and glutaric acid (59% and 82%, respectively). In turn, the lowest rate of cobalt recovery was obtained in sample 1 (1.5 M  $H_2SO_4 + H_2O_2$ ), despite the use of hydrogen peroxide as a reducing agent, which is often indicated in the literature as a compound that significantly improves the leaching of this metal [6]. The low cobalt recovery rate in the present experiments, despite the use of  $H_2O_2$ , can probably be explained by the application of too small of a dose of this factor. The preparation of the powder material for testing may also have had an impact—the entire electrode powder was used (i.e., anodic and cathodic mass) without additional thermal or chemical treatment, which is often practiced in literature sources to eliminate potential contamination, at the same time representing a more complicated material preparation process than the one presented in this paper. The use of organic acids as leaching agents affected the Li recovery rates—these results were much lower than for the sulfuric acid leach tests, while higher rates of this metal recovery were obtained for samples 5 and 6 leached with formic acid (47% and 45%, respectively). In the case of cobalt recovery, for samples 3–6, the rates were higher than for sample 1, but also lower than for sample 2. Among the experiments with organic acids, the best results for both tested metals were received for sample 6 (5 M  $CH_2O_2 + H_2O_2 + C_5H_8O_4$ )—Co: 26%, Li: 45%. Nevertheless, they are significantly lower than for a similar blend of reducing agents but combined with an inorganic leaching agent in the form of  $H_2SO_4$  (sample 2).

### 4. Conclusions

The obtained results of the conducted experiments on the acidic leaching of the electrode powder from spent Li-ion batteries indicate that it is possible to effectively recover the Li and Co metals contained in this type of waste material. The best results were received for the sample leached with inorganic sulfuric acid with the simultaneous use of two reducing agents: hydrogen peroxide and glutaric acid, which indicates the synergism of these two compounds in the acidic reaction environment. An alternative to the use of inorganic acids as leaching agents may be organic acids (e.g., lactic or formic acid), but the processes with their use require appropriate modeling and preliminary preparation of the research material to maximize the efficiency of the recovery of metals contained in the battery powder. The proposed method of obtaining metallic raw materials from spent batteries is in line with modern ideas of the circular economy model. It is also focused on the sustainable development and rational management of raw materials from natural resources, because after the selective separation process, the Co and Li from solutions gained following acidic leaching (e.g., in precipitation or solvent extraction processes) can be reused to produce, inter alia, new lithium-ion batteries.

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